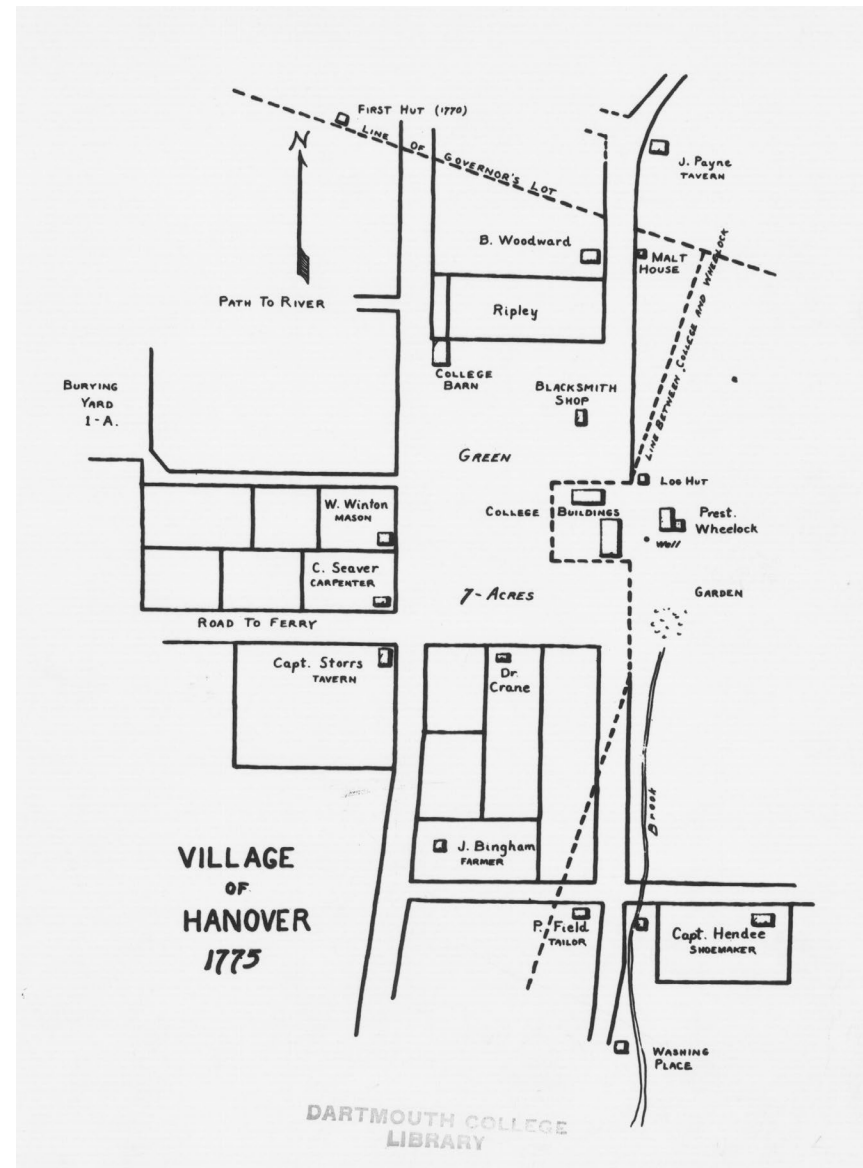




HANOVER DRINKING WATER

MEMBRANES & MILESTONES: HANOVER'S PATH TO PURE WATER







1868



1870

012808 DARTMOUTH COLLEGE FROM FAXON'S GARDEN.





- 1880 A DISASTROUS FIRE IN THE VILLAGE INDICATES THE NEED OF FIRE PROTECTION.
- 1887 PROFESSOR CHARLES PETTEE RECOMMENDS THAT THE VILLAGE BUILD A SYSTEM TO IMPOUND THE WATER OF CAMP BROOK AND CONSTRUCT A NEW DISTRIBUTION SYSTEM. THE STATE AUTHORIZES THE HANOVER VILLAGE PRECINCT TO RAISE \$20K (\$700K TODAY) TO IMPLEMENT PROFESSOR PETTEE'S PLAN. HOWEVER, THE AMOUNT IS INADEQUATE.
- 1890 ANOTHER SERIOUS FIRE EMPHASIZES THE NEED FOR FIRE PROTECTION.
- 1893 DARTMOUTH TRUSTEES AUTHORIZE AN APPROPRIATION OF \$25K TO CONSTRUCT THE PROPOSED PROJECT. (\$45K TODAY IS \$1.6M)
- 1893 THE HANOVER WATER WORKS COMPANY IS INCORPORATED ON AUGUST 1, 1893, AS A JOINT DARTMOUTH COLLEGE AND HANOVER VILLAGE PRECINCT COMPANY.



1893



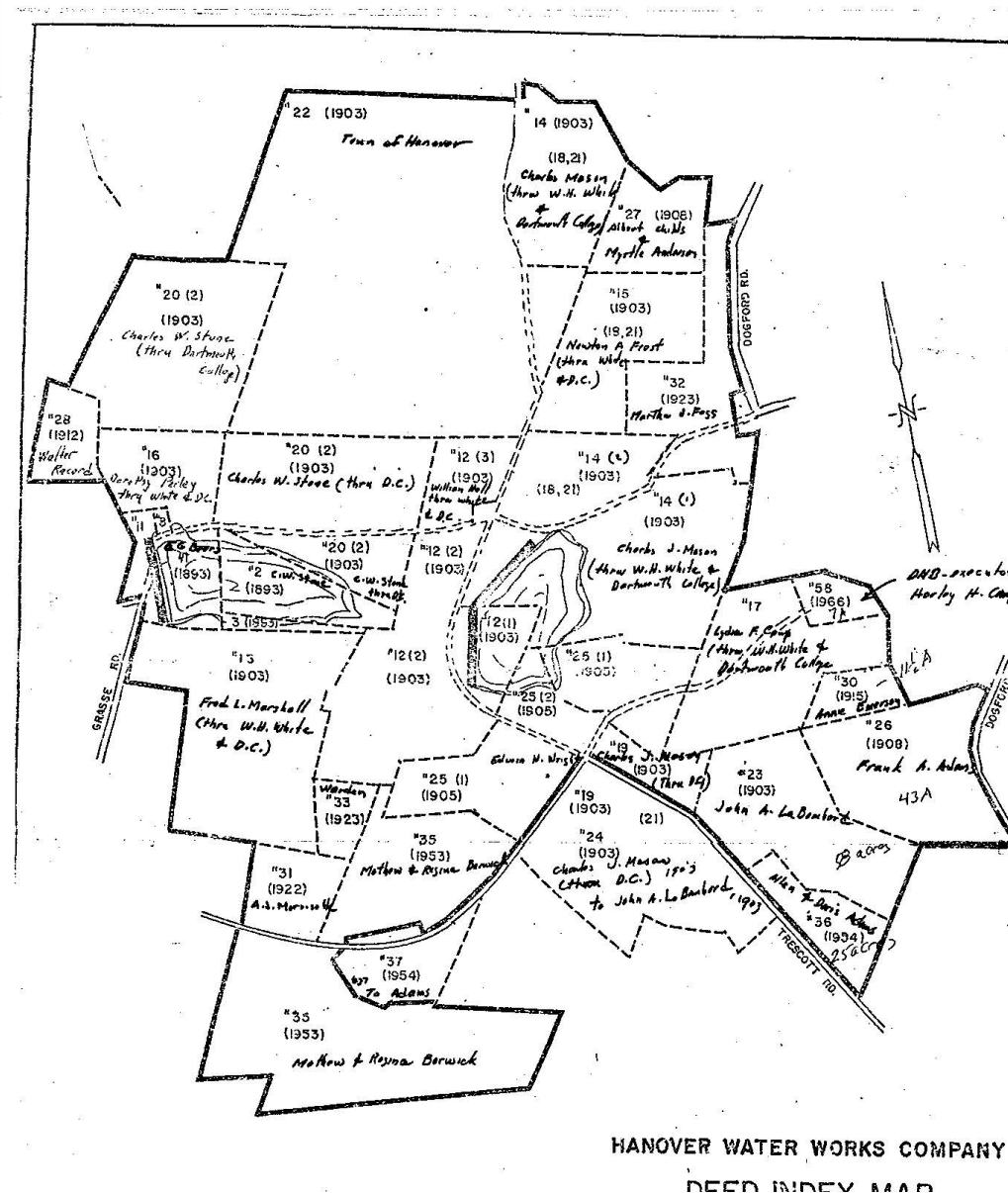









Health concern due to a 1903 Typhoid fever outbreak in Ithaca, NY (1,340 cases in a population of 3,000 people) prompted HWWCo to purchase all the land within the watershed.



Map Data Sources: Air photo: USDA, Roads: NH GRANIT, edited, also 2003 Hanover Master Plan; Property Boundary: Hanover Tax maps, GPO's, photo-interpretation



Map compiled for the Hanover Conservancy
by Stonehouse Mtn Mapping 
October, 2015

1915

The original reservoir level was raised to increase the impounded storage to 134,000,000 gallons.

1924

A second reservoir built on Camp Brook adds 150,000,000 gallons to impounded storage.

1951

The flow-line of the second reservoir raised increasing the impounded storage to 206,000,000 gallons.

1954

The capacity of the original reservoir increased to 219,000,000 gallons resulting in a total impounded storage 425,000,000 gallons.

1955

Continuous chlorination of supply commenced.

1958

After several public hearings, continuous fluoridation of the supply started.

1959

The installation of meters on all service lines commenced.

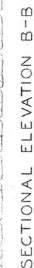
1962

A third reservoir was constructed on a tributary of Mink Brook in Hanover Center. increases storage to 525,000,000 gallons.



1924

SECTIONAL PLAN
PRESENT GATE CHAMBER



SCALE $\frac{3}{8}'' = 1' - 0''$
WESTON &
CONSULTING





1962

CONTRACT NO.1

**CHLORINE DIOXIDE DISINFECTION
SYSTEM**

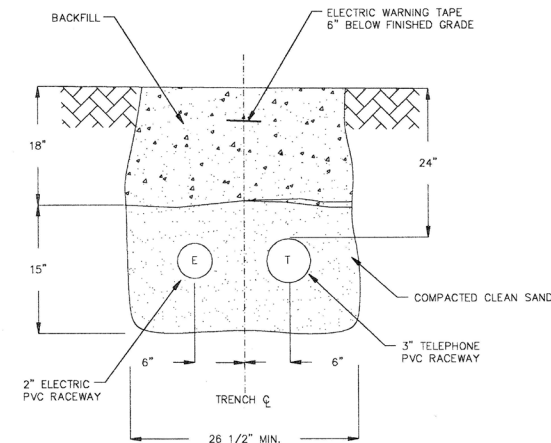
**HANOVER WATER WORKS COMPANY
HANOVER, NEW HAMPSHIRE**

BOSTON, MA



Proj No	6948
Scale	1"=20'
Drawn By	PJF
Ens. By	DSG
Checkd. By	EPD
Appd. By	SAC
Date	MAY 21, 1993

Date	Description
UTILITY RELOCATION & PIPING PLAN	

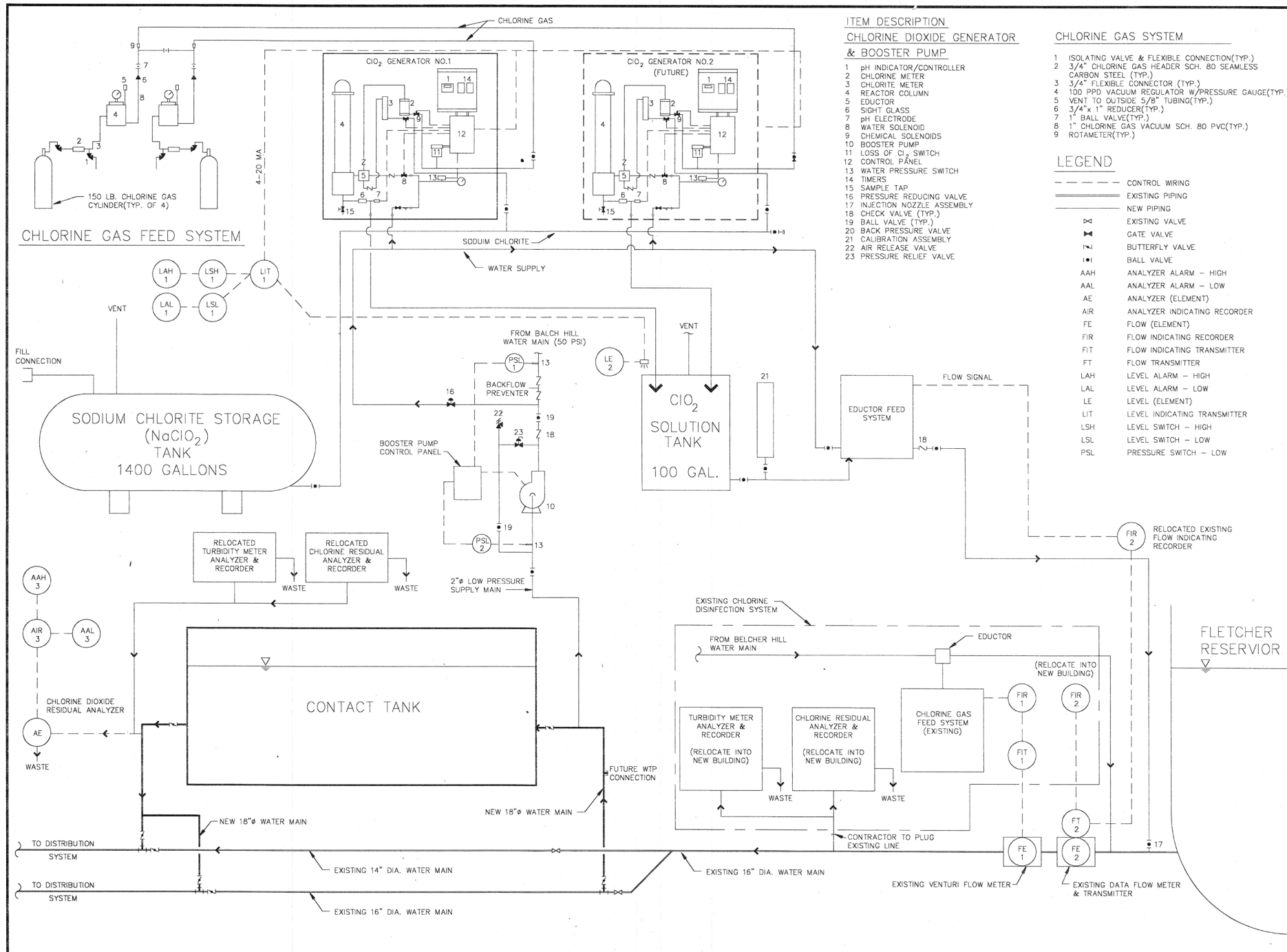


SECTION A-A

N O T E S :

1. SEE SHEET No. C-1 FOR GENERAL NOTES & LEGEND.
2. THE CONTRACTOR SHALL MAINTAIN FLOW IN EITHER THE 14" OR 16" WATER MAINS AT ALL TIMES. NO WATER MAIN SHALL BE REMOVED FROM SERVICE WITHOUT WRITTEN APPROVAL FROM HANOVER WATER WORKS CO.
3. DEFLECT PIPE JOINTS OR PROVIDE ADDITIONAL PIPE BENDS IN VERTICAL PLANE AS REQUIRED TO MAINTAIN THE SPECIFIED COVER OVER THE PIPE.
4. NEW VALVE INSTALLATION & PIPE CONNECTIONS ARE TO BE MADE IN THE DRY. REMOVE SECTIONS OF 14" & 16" PIPE AS REQUIRED AND REPLACE WITH NEW PIPE & FITTINGS. (SEE NOTE No. 10 ABOVE). INVERT ELEVATION OF 14" PIPE SHALL BE LOWERED TO ALLOW NEW 18" CONNECTION TO 16" PIPE TO PASS OVER IT.
5. DRAIN LINE FROM WATER SERVICE BUILDING TO CATCH BASIN TO BE 3'-0" BELOW GRADE.
6. 4" PVC CONDUIT TO BE BURIED 5'-0" BELOW GRADE AND BE SCHEDULE 80 ELECTRICAL CONDUIT WITH 24" RADIUS BENDS. INSTALL A PULLING WIRE AT TIME OF INSTALLATION.
7. COPPER SAMPLE PIPE TO BE BURIED 5'-0" BELOW GRADE.
8. PIPE RESTRAINT SHALL BE ACCOMPLISHED BY USING JOINT RESTRAINTS.
9. REFER TO ELECTRICAL DRAWINGS FOR CONDUIT SIZE AND WIRE FOR NEW UNDERGROUND ELECTRIC LINES.

1993



ITEM DESCRIPTION
CHLORINE DIOXIDE GENERATOR
& BOOSTER PUMP

- 1 pH INDICATOR/CONTROLLER
- 2 CHLORINE METER
- 3 CHLORITE METER
- 4 REACTOR COLUMN
- 5 EDUCTOR
- 6 SIGHT GLASS
- 7 pH ELECTRODE
- 8 WATER SOLENOID
- 9 CHEMICAL SOLENOIDS
- 10 BOOSTER PUMP
- 11 LOSS OF Cl_2 SWITCH
- 12 CONTROL PANEL
- 13 WATER PRESSURE SWITCH
- 14 TIMERS
- 15 SAMPLE TAP
- 16 PRESSURE REDUCING VALVE
- 17 INJECTION NOZZLE ASSEMBLY
- 18 CHECK VALVE (TYP.)
- 19 BALL VALVE (TYP.)
- 20 BACK PRESSURE VALVE
- 21 CALIBRATION ASSEMBLY
- 22 AIR RELEASE VALVE
- 23 PRESSURE RELIEF VALVE

CHLORINE GAS SYSTEM

- 1 ISOLATING VALVE & FLEXIBLE CONNECTION (TYP.)
- 2 3/4" CHLORINE GAS HEADER SCH. 80 SEAMLESS
- 3 CARBON STEEL (TYP.)
- 4 3/4" FLEXIBLE CONNECTOR (TYP.)
- 5 100 PPD VACUUM REGULATOR W/PRESSURE GAUGE (TYP.)
- 6 VENT TO OUTSIDE 5/8" TUBING (TYP.)
- 7 3/4" x 1" REDUCER (TYP.)
- 8 1" CHLORINE GAS VACUUM SCH. 80 PVC (TYP.)
- 9 ROTAMETER (TYP.)

LEGEND

- CONTROL WIRING
- EXISTING PIPING
- NEW PIPING
- EXISTING VALVE
- GATE VALVE
- BUTTERFLY VALVE
- BALL VALVE
- AAH ANALYZER ALARM - HIGH
- AAL ANALYZER ALARM - LOW
- AE ANALYZER (ELEMENT)
- AIR ANALYZER INDICATING RECORDER
- FE FLOW (ELEMENT)
- FIR FLOW INDICATING RECORDER
- FIT FLOW INDICATING TRANSMITTER
- FT FLOW TRANSMITTER
- LAH LEVEL ALARM - HIGH
- LAL LEVEL ALARM - LOW
- LE LEVEL (ELEMENT)
- LIT LEVEL INDICATING TRANSMITTER
- LSH LEVEL SWITCH - HIGH
- LSL LEVEL SWITCH - LOW
- PSL PRESSURE SWITCH - LOW

CONTRACT NO.1

CHLORINE DIOXIDE DISINFECTION SYSTEM

HANOVER WATER WORKS COMPANY
HANOVER, NEW HAMPSHIRE

Anderson-Nichols

engineers
environmental consultants
architects

BOSTON, MA

PROCESSED

RECEIVED FOR ADDITIONAL CHARGE ORDER NO. 1

DATE

BY

REMARKS

DATE

BY

REMARKS

DATE

BY

REMARKS

PI-1






Town of Hanover
Hanover Water Company
Water Quality Parameters

Turbidity (NTU)

As of 5/19/04		CRREL					COMMUNITY CENTER		
Date	Raw	Contact Tank	Kendal	Fire Station	Kellogg Building	Fairbanks	Food Stop	Hopkins Center	High School
01/06/04	0.79	1.01	0.96	1.04	1.02	1.22	0.98	1.49	1.06
01/20/04	0.63	0.83	0.89	0.74	0.67	0.70	0.64	*5.63	0.77
02/03/04	0.69	1.12	0.82	0.82	0.87	0.91	0.92	1.19	0.99
02/19/04	0.92	0.96	1.11	1.14	1.00	0.89	1.08	1.89	0.87
03/02/04	0.61	0.75	1.00	0.78	0.83	0.83	1.39	1.54	0.89
03/23/04	0.56	0.99	0.75	0.96	0.66	0.86	0.91	1.64	0.80
04/06/04	1.02	1.38	1.13	1.18	1.53	1.48	1.11	1.84	0.98
04/20/04	1.13	1.30	1.36	1.38	1.66	1.63	1.52	2.25	1.42
05/03/04	1.27	1.61	1.20	1.29	2.17	1.08	1.19	1.24	0.95
05/19/04	0.69	0.79	0.77	0.66	0.74	0.81	0.65	1.15	0.88
06/01/04	0.87	0.81	0.95	0.84	0.99	0.88	1.05	1.10	0.76
06/15/04	0.92	0.89	0.99	1.16	1.27	0.80	1.00	0.91	0.79
07/06/04	0.94	1.10	1.69	1.19	1.05	1.10	1.13	1.26	1.53
07/21/04	0.86	0.78	0.99	0.88	0.87	0.80	0.92	1.36	0.79
08/10/04	0.98	0.82	1.38	0.86	0.87	0.80	0.81	1.16	0.77
08/17/04	0.68	0.59	0.83	0.64	0.91	0.89	0.68	1.20	0.82
09/07/04	0.69	0.71	0.92	0.65	0.70	0.60	0.65	1.36	0.68
09/21/04	0.85	0.67	1.07	1.14	0.84	0.77	0.88	1.03	1.05
10/04/04	1.05	0.95	0.83	0.77	0.89	0.83	0.81	1.05	0.86
10/19/04	1.17	1.33	1.44	1.40	1.37	1.23	1.36	1.55	1.19
11/09/04	1.21	1.29	1.31	1.30	1.29	1.18	1.29	0.14	1.09
11/23/04	0.72	0.89	1.18	0.95	1.04	0.96	0.90	0.96	1.05
12/14/04	0.84	0.81	0.96	0.87	0.93	0.81	0.83	1.05	0.85
12/21/04	0.79	0.95	0.94	0.89	0.95	0.96	0.90	0.95	0.91
Average	0.87	0.97	1.06	0.98	1.05	0.96	0.98	1.27	0.95
High	1.27	1.61	1.69	1.38	2.17	1.63	1.52	2.25	1.53
Low	0.56	0.75	0.75	0.66	0.66	0.70	0.64	0.91	0.76



Still had the following issues

- TASTE AND ODOR COMPLAINTS
 - COMPLIANCE WITH THE LEAD AND COPPER RULE
 - COMPLIANCE WITH CURRENT AND PROPOSED SURFACE WATER RULES AND REGULATIONS.
 - SAFE YIELD REDUCED DUE TO REQUIRED CHLORINE CONTACT REQUIREMENTS AND NO POST TREATMENT STORAGE IN THE MAIN SYSTEM
- 



Options considered:

No Filtration


Ground Water – TCE present in ground water near CRREL, high iron & manganese.

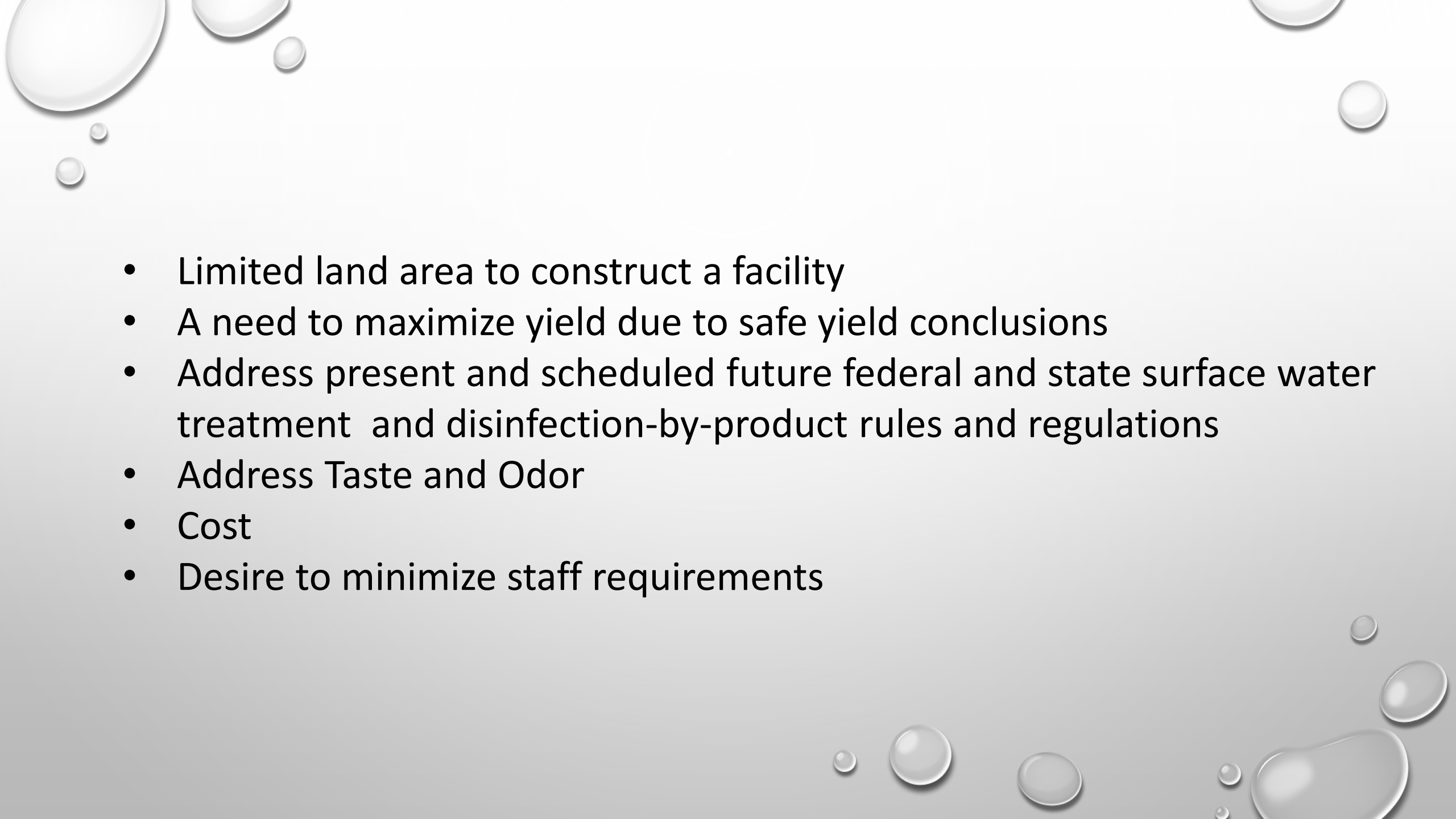
Conventional Filtration – more economical > 10 MGD, higher capital cost and larger land area required.

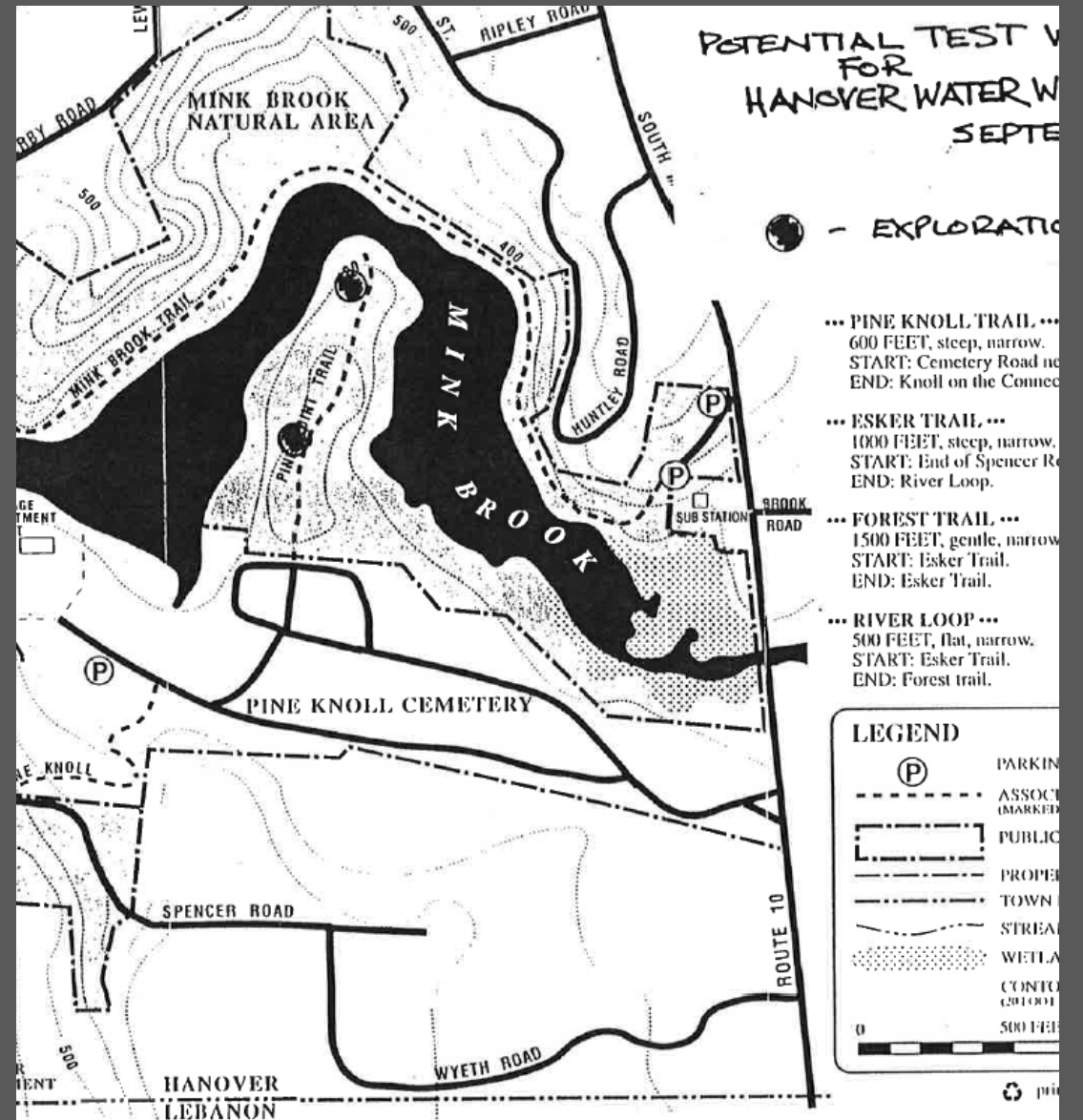
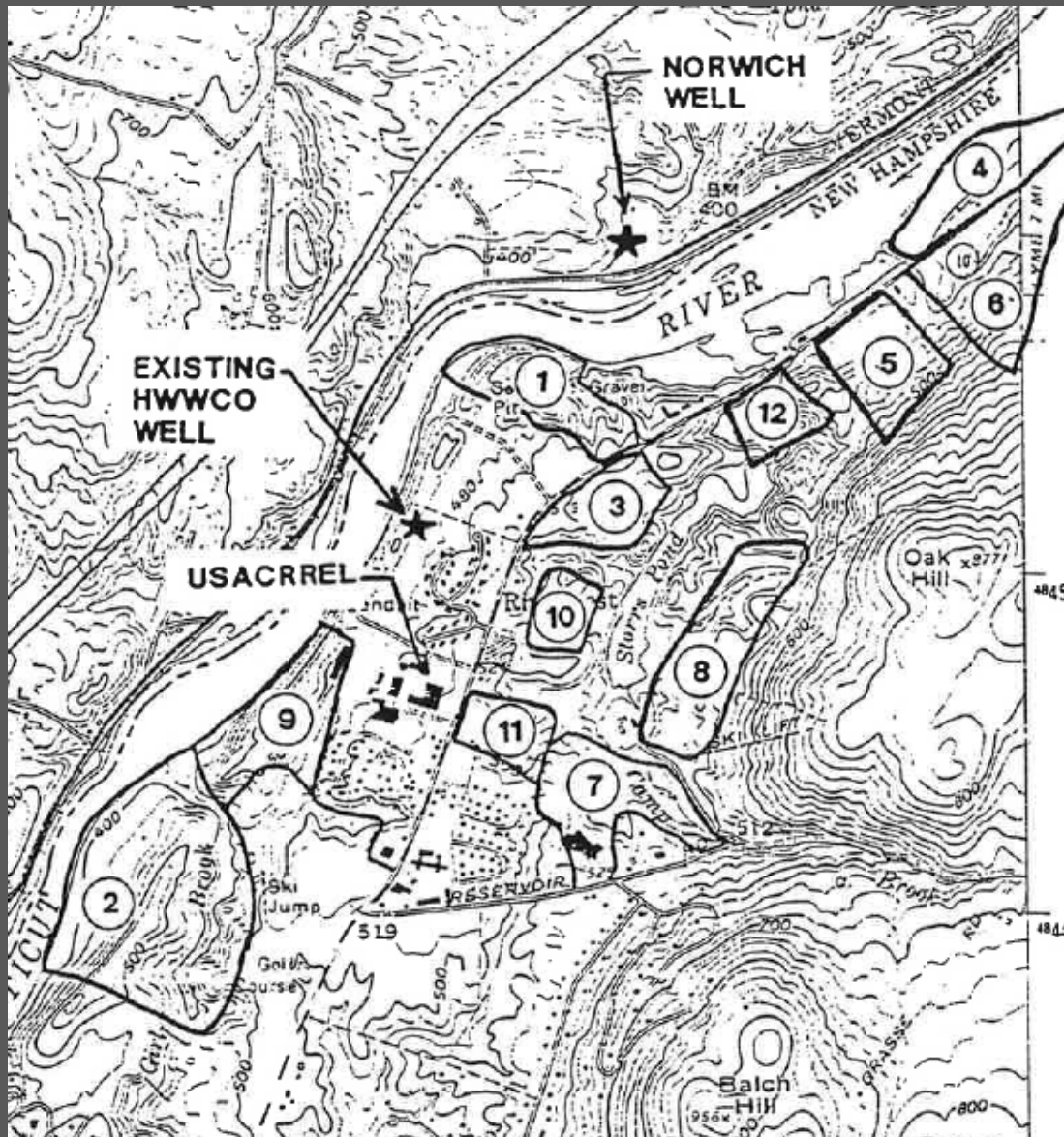
Slow Sand Filtration, color < 10, < 5 NTU, ineffective at removal of TOC, can get higher with Granular Activated Carbon (GAC) and pre-ozonation

Package Filtration packaged mixed media – 10 NTU limit, alkalinity < 20 mg/l, color < 60

Membrane filtration – 6 log removal of giardia & cryptosporidium, color, iron & manganese, THM precursors, TOC, 0.1 micron pore size. Effective at removing higher turbidity levels (450 NTU)



- 
- Limited land area to construct a facility
 - A need to maximize yield due to safe yield conclusions
 - Address present and scheduled future federal and state surface water treatment and disinfection-by-product rules and regulations
 - Address Taste and Odor
 - Cost
 - Desire to minimize staff requirements





Filtration Technology Comparison

- Kinetico Pressure Vessel Filtration System
 - U.S. Filter Microfloc “Trident” System
 - Pall Membrane “Aria” Microfiltration System
- 

Screening and Rank of Alternatives

Criteria	Points	<i>OPTION 1</i> KINETICO FILT RATION ¹	<i>OPTION 2</i> PACKAGED MICROFLOC ¹	<i>OPTION 3</i> MEMBRANE MICRO FILTRATION
Health and Safety	1-5	5	5	5
Equipment Cost	1-5	2	3	4
O & M Cost	1-5	2	3	4
Meets LT2SWTR Rule	1-5	4	4	5
Addresses Primary Contaminant Issues	1-5	4	4	4
Meets Disinfection By-Product Rule	1-5	4	4	4
Additional Land Required	1-5	4	4	5
Water Use Efficiency	1-5	4	4	4
Ease of Operation	1-5	3	3	4
Power Requirements	1-5	4	4	2
Hazardous Chemical Handling	1-5	4	4	3
Waste Generation	1-5	3	3	4
Totals	12-60	43	45	48

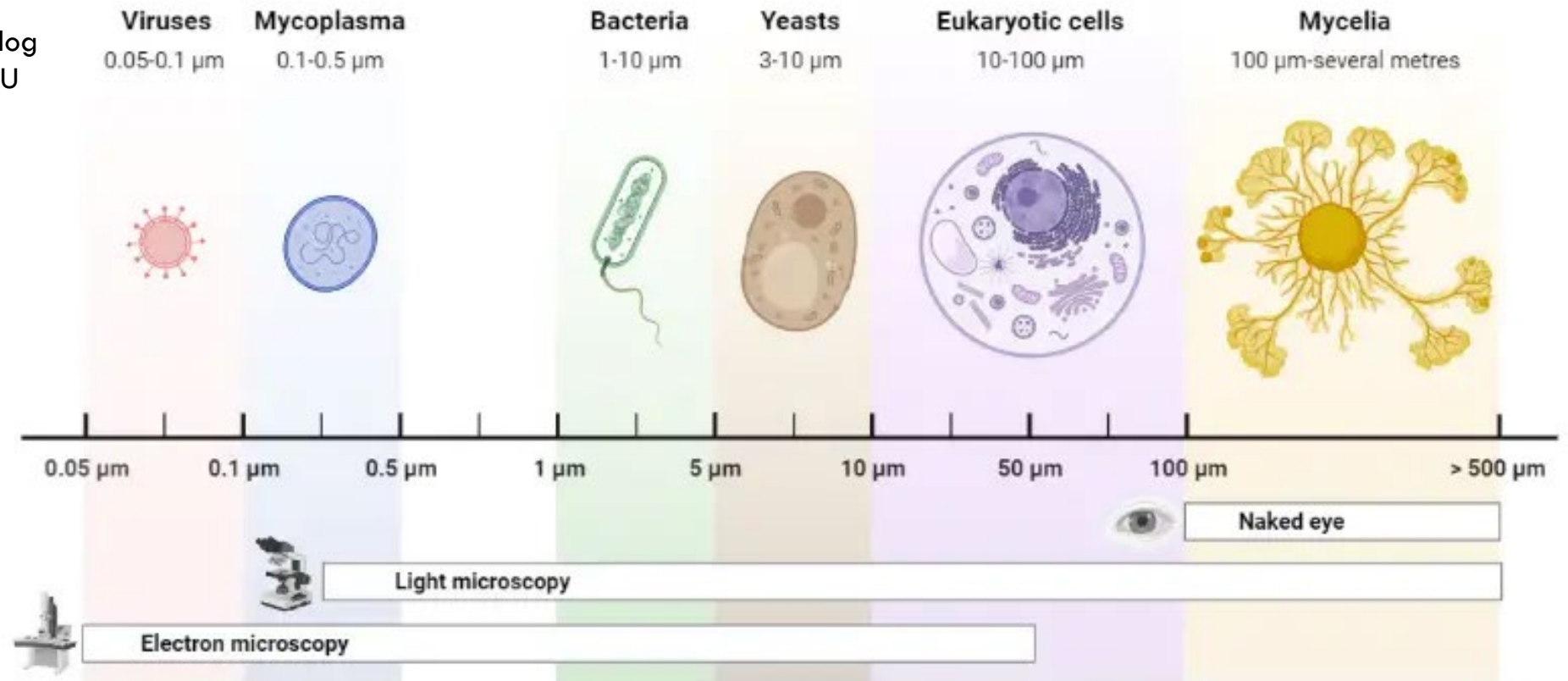
Primary Contaminant Treatment Comparison

Contaminant	MF Removal	Package Treatment Removal
Viruses	1-2.5 log	1-log
Cryptosporidium Oocysts	6-log	2.5-3.0-log
Giardia Cysts	6-log	2.5-log
Fecal Coliforms	6-log	3.0-4.0-log
Turbidity	0.04-0.1 NTU	0.08-0.3 NTU
Dissolved Metals	1.0-2.0-log	1.0-2.0-log
Dissolved Natural Organic Matter	40-60 Percent	40-70 Percent

Membrane Filtration

Contaminate	Typical removal
Giardia	> 6 log
Cryptosporidium	> 6 log
E. Coli	0.5 - 3 log
Turbidity	<0.1 NTU

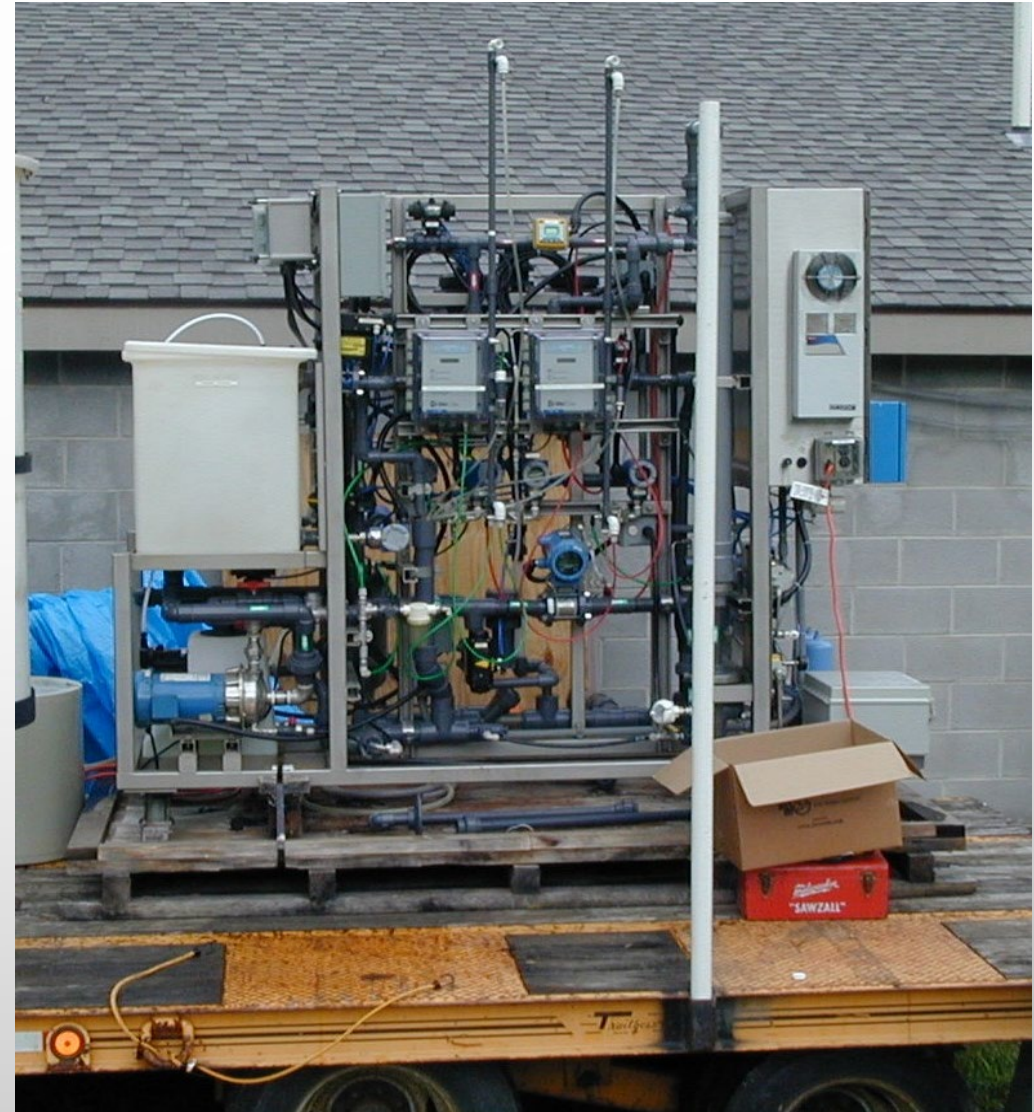
Size of Representative Bacteria, Viruses, Yeasts and Eukaryotic Cells



US Filter Memcor



Pall Aria



PARALLEL PILOTS



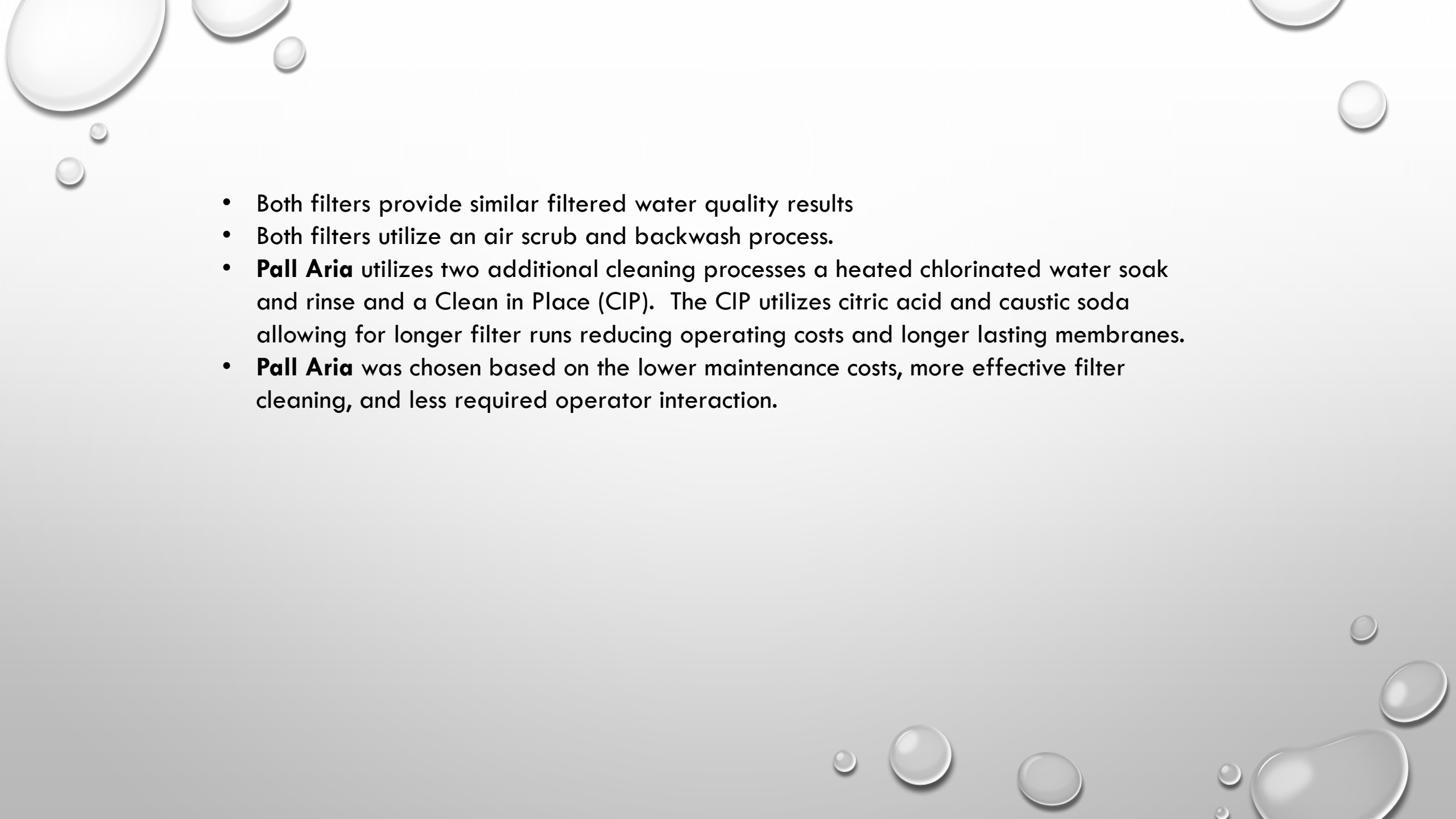
PRETREATMENT AND COMPRESSOR SYSTEM



PHASE 1
(NO
PRETREATMENT) LAB
RESULTS

PARAMETER	FEED WATER		PALL AND U.S. FILTER FILTRATE	
	Concentration Range	Average Concentration	Concentration Range	Average Concentration
Turbidity (NTU)	0.331 – 0.421	0.367	0.021 – 0.027	0.024
Color (CU)	3 – 23	11.6	0 – 21	9.5
Iron (mg/L)	0.02 – 0.05	0.04	0.00 – 0.01	0.004
Manganese (mg/L)	0.006 – 0.078	0.015	0.000 – 0.007	0.001
Hardness (mg/L)	18– 21	19.4	17 – 22	19.7
TDS (mg/L)	43-49	45.9	41 – 48	42.3
Alkalinity (mg/L)	12.0 – 18.5	14.6	13.5 – 15.0	14.4
pH	6.8 – 7.5	7.05	6.9 – 7.4	7.08

PARAMETER

- 
- Both filters provide similar filtered water quality results
 - Both filters utilize an air scrub and backwash process.
 - **Pall Aria** utilizes two additional cleaning processes a heated chlorinated water soak and rinse and a Clean in Place (CIP). The CIP utilizes citric acid and caustic soda allowing for longer filter runs reducing operating costs and longer lasting membranes.
 - **Pall Aria** was chosen based on the lower maintenance costs, more effective filter cleaning, and less required operator interaction.

Raw water filtered without coagulant

TABLE B-5
Phase 1 Daily Water Quality Data
On Site Analysis – August 26 through September 15, 2003

Date	Turbidity		Color		Iron		Manganese		Alkalinity		pH	
	Feed	Filtrate	Feed	Filtrate	Feed	Filtrate	Feed	Filtrate	Feed	Filtrate	Feed	Filtrate
8/26/03	0.419	0.021	6	0	0.03	0.00	0.078	0.000	16	15	7.22	7.23
8/27/03	0.421	0.021	13	15	0.04	0.01	0.009	0.001	14	14	6.85	6.98
8/28/03	0.377	0.022	14	12	0.03	0.00	0.014	0.007	13	13.5	7.12	7.25
8/29/03	0.372	0.027	7	10	0.05	0.00	0.011	0.001	12	14.5	6.95	7.02
9/02/03	0.339	0.021	7	0	0.02	0.00	0.019	0.001	15	15.5	7.13	7.10
9/03/03	0.351	0.022	18	17	0.05	0.01	0.012	0.000	14.5	13.5	6.83	6.88
9/04/03	0.337	0.027	15	9	0.04	0.01	0.009	0.001	13.5	14.5	7.16	6.93
9/05/03	0.353	0.021	12	10	0.04	0.01	0.008	0.001	15	15	6.72	6.87
9/08/03	0.331	0.021	9	14	0.03	0.00	0.009	0.001	15	14.5	6.84	6.75
9/09/03	0.342	-	10	-	0.04	-	0.011	-	14.5	-	6.81	-
9/10/03	0.358	0.027	3	3	0.04	0.01	0.006	0.001	18.5	14.0	7.35	7.37
9/11/03	0.370	0.027	21	3	0.03	0.00	0.010	0.001	15.0	14.5	7.52	7.42
9/12/03	0.383	0.027	5	21	0.03	0.00	0.010	0.001	15.0	14.0	7.18	7.26
9/15/03	0.387	0.027	23	10	0.03	0.00	0.010	0.001	15.0	15.0	7.02	6.96
Average	0.367	0.024	11.6	9.5	0.04	0.004	0.015	0.001	14.6	14.4	7.05	7.08

Phase 1 Lab results

Parameter	Location		
	Raw Water	Pall MF Filtrate	US Filter MF Filtrate
Total Suspended Solids (mg/L)	<4	<4	<4
Color (CU)	15	5	5
Total Iron (mg/L)	0.09	<0.02	0.03
Total Manganese (mg/L)	0.04	0.03	<0.02
Total Organic Carbon (mg C/L)	4.2	4.0	4.3
Dissolved Organic Carbon (mg C /L)	4.8	3.8	3.7
THM Formation Potential (ppb)	103.6	-	90.7
Total Coliforms	Present	Absent	Absent
E. Coli	Present	Absent	Absent

PHASE 2 (PRETREATMENT WITH PACL) RESULTS

Parameter	Feed Water		Pall and U.S. Filter Filtrate	
	Concentration Range	Average Concentration	Concentration Range	Average Concentration
Turbidity (NTU)	1.307 – 10.72	2.393	0.026 - 0.033	0.028
Color (CU)	1 - 23	15.8	0	0
Iron (mg/L)	0.06 – 0.19	0.10	0.00 – 0.02	0.01
Manganese (mg/L)	0.006 – 0.154	0.043	0.000 – 0.070	0.030
Hardness (mg/L)	16.5 – 20.1	18.2	16.0 – 19.0	18.1
TDS (mg/L)	35 - 37	35.3	42 - 46	43.5
Alkalinity (mg/L)	12.5 – 15.0	14.1	10.0 – 12.0	11.3
pH	6.42 – 6.98	6.69	6.22 – 6.96	6.65

PHASE 2 TOC RESULTS

Parameter	Location	
	Pall MF Raw Water	Pall MF Filtrate
Total Organic Carbon (mg C/L) (1.8 mg/L as AL)	3.3	1.9
Total Organic Carbon (mg C/L) (2.2 mg/L as AL)	3.4	1.8

Table B-10
Phase 2 Daily Water Quality Data
On Site Analyses – October 7 through November 6, 2003

Date	Turbidity		Color		Iron		Manganese		Alkalinity		pH	
	Feed	Filtrate	Feed	Filtrate	Feed	Filtrate	Feed	Filtrate	Feed	Filtrate	Feed	Filtrate
Polyaluminum Chloride (Holland Co. PCH-101) Dosage Equals 10 mg/L as Aluminum												
10/07/03	1.134	0.022	24	5	0.13	0.00	0.052	0.068	7.0	7.0	6.64	6.53
10/08/03	1.253	0.020	28	6	0.10	0.00	0.052	0.067	15.0	7.6	6.78	6.63
10/09/03	1.758	0.021	16	2	0.22	0.01	0.037	0.056	14.0	14.0	6.61	6.32
10/10/03	1.134	0.021	18	4	0.19	0.01	0.039	0.052	14.5	14.5	6.65	6.61
10/11/03	1.184	0.020	5	0	0.10	0.00	0.046	0.058	6.5	7.0	6.57	6.48
10/12/03	1.067	0.020	9	0	0.12	0.02	0.050	0.054	9.5	8.0	6.71	6.48
10/13/03	1.125	0.020	12	4	0.19	0.00	0.057	0.054	6.5	6.5	6.22	6.22
Polyaluminum Chloride (Holland Co. PCH-180) Dosage Equals 5 mg/L as Aluminum												
10/20/03	1.173	0.020	18	0	0.15	0.00	0.043	0.040	7.5	5.5	6.55	6.36
10/21/03	0.834	0.020	25	0	0.17	0.01	0.031	0.001	-	-	6.65	7.00
10/22/03	1.108	0.021	11	0	0.11	0.00	0.020	0.037	8.0	9.0	6.34	6.37
10/23/03	1.205	0.021	16	0	0.14	0.02	0.027	0.034	8.5	9.0	6.74	6.68
10/24/03	1.685	0.021	11	0	0.16	0.00	0.014	0.031	10.5	11.5	7.22	7.07
10/27/03	2.440	0.021	4	0	0.09	0.00	0.013	0.010	11.0	10.0	6.51	6.50
10/28/03	0.985	0.021	27	13	0.10	0.00	0.015	0.038	11.5	10.0	6.53	6.57
10/29/03	1.211	0.021	17	0	0.11	0.01	0.113	0.037	11.0	9.5	6.29	6.48
10/30/03	1.110	0.021	14	8	-	-	0.032	0.036	-	-	6.75	6.76
10/31/03	2.719	0.021	52	0	-	-	0.038	0.029	-	-	6.55	6.64
11/03/03	1.164	0.021	28	0	0.11	0.00	0.029	0.039	13.0	13.0	7.02	6.94
11/05/03	3.261	0.021	61	12	0.22	0.00	0.040	0.037	14.5	12.5	7.27	7.21
11/06/03	1.642	0.021	17	0	0.11	0.00	0.044	0.034	-	17.0	6.97	7.05

Phase 2 addition of PAC for disinfection byproduct and color removal

Table B-11
Phase 2 Daily Water Quality Data
On Site Analysis – December 6 through 17, 2003

Date	Turbidity		Color		Iron		Manganese		Alkalinity		pH	
	Feed	Filtrate	Feed	Filtrate	Feed	Filtrate	Feed	Filtrate	Feed	Filtrate	Feed	Filtrate
Polyaluminum Chloride (Holland Co. PCH-180) Dosage Equals 2.2 mg/L as Aluminum												
12/06/03	1.597	0.027	23	0	0.18	0.00	0.051	0.070	12.5	10.0	6.42	6.38
12/07/03	1.455	0.026	12	0	0.11	0.02	0.154	0.034	14.0	11.0	6.74	6.71
12/08/03	1.616	0.026	18	0	0.06	0.00	0.026	0.028	14.0	10.5	6.55	6.60
12/09/03	1.436	0.026	1	0	0.07	0.01	0.006	0.000	14.0	11.0	6.93	6.78
12/10/03	10.72	0.026	14	0	0.08	0.00	0.042	0.032	14.5	12.0	6.98	6.97
12/11/03	1.787	0.027	22	0	0.19	0.02	0.028	0.028	13.5	12.0	6.96	6.96
Polyaluminum Chloride (Holland Co. PCH-180) Dosage Equals 1.8 mg/L as Aluminum												
12/12/03	1.387	0.031	15	0	0.08	0.00	0.020	0.022	14.0	11.0	6.74	6.69
12/15/03	1.310	0.033	16	0	0.08	0.00	0.037	0.029	15.0	12.0	6.57	6.55
12/16/03	1.316	0.031	20	0	0.08	0.01	0.030	0.028	14.5	11.0	6.44	6.22
12/17/03	1.307	0.031	17	0	0.09	0.00	0.034	0.024	15.0	12.0	6.54	6.59
Average	2.393	0.028	15.8	0	0.10	0.01	0.043	0.030	14.1	11.3	6.69	6.65

Phase 2 addition of PAC for disinfection byproduct and color removal
based on pilot expected 30 hrs at 1.8-2.2 mg/l of PAC before CIP



DURING DESIGN THIS HAPPENED

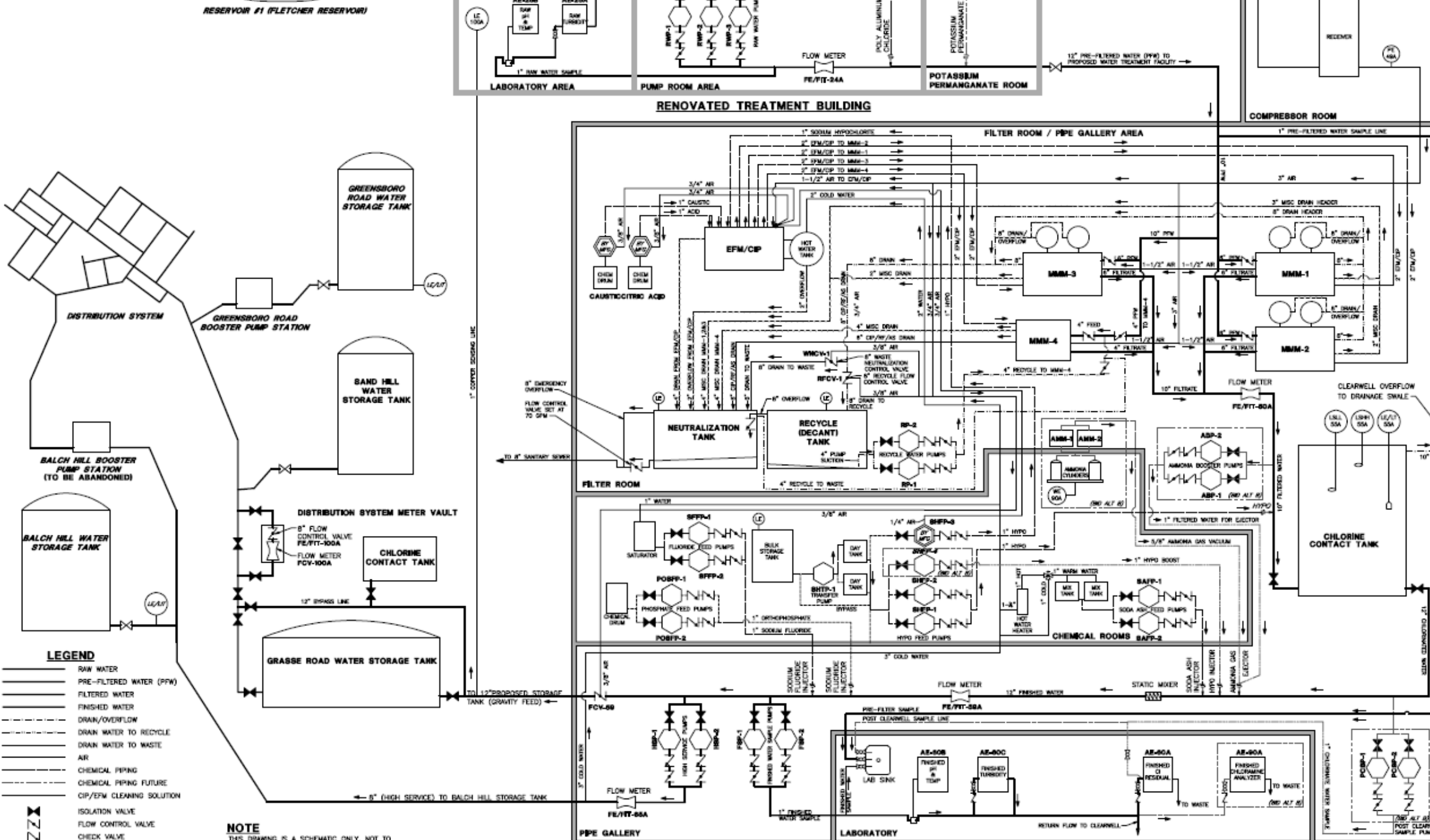
JUNE 10, 2005

Town of Hanover
Hanover Water Company
Water Quality Parameters

Turbidity (NTU)

Date	Raw	Contact	CRREL	Fire	Kellogg	Fairbanks	Food	Hopkins	High
		Tank		Station	Building		Stop	Center	School
01/04/05	0.57	0.77	0.88	0.83	1.03	0.84	0.85	0.99	1.06
01/26/05	0.57	0.78	0.87	0.76	0.81	0.86	0.82	0.82	0.79
02/01/05	0.73	0.84	0.96	0.84	0.99	0.92	0.91	0.99	0.75
02/23/05	0.47	0.80	0.86	0.90	0.84	0.87	0.82	0.78	0.76
03/08/05	0.41	0.56	0.81	0.85	0.62	0.77	0.60	0.68	0.69
03/22/05	0.57	0.56	0.76	0.52	0.57	0.58	0.52	0.59	0.49
04/05/05	1.58	2.09	1.78	1.84	1.86	1.78	1.74	1.72	0.71
04/21/05	1.90	1.64	1.98	3.51	1.88	1.73	1.56	1.79	1.59
05/04/05	1.14	1.21	1.30	1.12	1.15	1.10	1.02	1.37	1.15
05/18/05	0.63	0.57	0.73	0.55	0.75	0.55	0.53	0.69	0.57
06/01/05	0.77	0.70	0.71	0.66	0.68	0.68	0.60	0.86	0.67
06/13/05	46.00	9.25	22.20	13.10	21.30	17.90	12.70	16.50	4.53
07/12/05	5.18	4.14	6.08	8.86	12.00	4.54	4.17	4.68	3.77
07/25/05	1.81	2.54	2.85	2.38	5.46	2.77	3.07	2.99	2.12
08/02/05	NA	NA	NA	NA	NA	NA	NA	NA	NA
08/23/05	0.93	1.30	3.82	1.75	1.97	3.16	2.19	1.04	2.26
09/06/05	1.22	0.88	1.38	1.00	1.59	0.96	1.24	1.14	1.20
09/20/05	1.75	1.08	5.19	2.86	1.02	0.93	1.58	1.40	0.89
10/06/05	0.95	0.83	2.37	2.47	1.25	2.06	1.32	1.53	0.73
10/26/05	1.46	1.68	2.02	1.71	1.57	1.77	1.78	1.95	1.27
11/01/05	1.48	1.51	1.60	1.50	1.48	1.47	1.50	1.62	1.55
11/15/05	NA	NA	NA	NA	NA	NA	NA	NA	NA
12/06/05	3.25	1.56	2.11	1.86	3.15	1.78	2.11	3.65	1.04
12/15/05	1.34	1.35	1.92	1.59	1.56	1.30	1.72	2.26	1.07
Average	3.40	1.67	2.87	2.34	2.89	2.24	1.97	2.27	1.35
High	46.00	9.25	22.20	13.10	21.30	17.90	12.70	16.50	4.53
Low	0.41	0.56	0.71	0.52	0.57	0.55	0.52	0.59	0.49

RESERVOIR #1 (FLETCHER RESERVOIR)



LEGEND

- RAW WATER
- PRE-FILTERED WATER (PFW)
- FILTERED WATER
- FINISHED WATER
- DRAIN/OVERFLOW
- DRAIN WATER TO RECYCLE
- DRAIN WATER TO WASTE
- AIR
- CHEMICAL PIPING
- CHEMICAL PIPING FUTURE
- CIP/EFM CLEANING SOLUTION
- ISOLATION VALVE
- FLOW CONTROL VALVE
- CHECK VALVE
- PUMP

NOTE

THIS DRAWING IS A SCHEMATIC ONLY. NOT TO BE USED FOR CONSTRUCTION. ACTUAL PIPING SIZES AND CONNECTIONS SHOWN ON PROCESS PIPING DRAWINGS ARE TO PREVAIL.

REVISION	DATE	BY	CHKD	APP'D	PROJECT NO.	SCALE
1	10/1/00	JL	AL	AL	100-000000	1/4" = 1'-0"
2	10/1/00	JL	AL	AL	100-000000	1/4" = 1'-0"
3	10/1/00	JL	AL	AL	100-000000	1/4" = 1'-0"
4	10/1/00	JL	AL	AL	100-000000	1/4" = 1'-0"
5	10/1/00	JL	AL	AL	100-000000	1/4" = 1'-0"
6	10/1/00	JL	AL	AL	100-000000	1/4" = 1'-0"
7	10/1/00	JL	AL	AL	100-000000	1/4" = 1'-0"
8	10/1/00	JL	AL	AL	100-000000	1/4" = 1'-0"
9	10/1/00	JL	AL	AL	100-000000	1/4" = 1'-0"
10	10/1/00	JL	AL	AL	100-000000	1/4" = 1'-0"

HANOVER WATER WORKS COMPANY
HANOVER, NEW HAMPSHIRE
CONTRACT 1
MEMBRANE FILTRATION FACILITY
PROCESS FLOW DIAGRAM

DWG PR-2
33 OF 70







